

# NORTH CAROLINA D.O.T. PEDESTRIAN FERRY

Mechanical Calculations

Prepared for: NCDOT • Raleigh, NC

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#### PREPARED BY

#### Elliott Bay Design Group – North Carolina, PLLC 5305 Shilshole Ave. NW, Ste. 100 Seattle, WA 98107

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## 1 PURPOSE

This report documents the calculations used in support of piping and machinery system designs for the North Carolina D.O.T. Pedestrian Ferry. The subject vessel is a new design for a 92 ft long x 26 ft wide, catamaran type, fast passenger ferry, which will be owned and operated by the North Carolina Department of Transportation (NCDOT).

The calculations relating to each specific system are presented in separate appendices. Each appendix provides the following information:

- References used in preparing the calculations
- Description of the system
- Calculation procedures
- Given and assumed parameters
- Formulas and software used
- Calculation results

### 2 REGULATORY FRAMEWORK

The Pedestrian Ferry is inspected by the US Coast Guard under the provisions of 46 CFR Subchapter T. The vessel structure and bilge system are designed in accordance with Lloyd's Register Rules and Regulations for the Classification of Special Service Craft, 2016. Therefore, all piping and mechanical system design shall comply with the respective requirements of these agencies.

# Appendix A

HVAC

## **1 DESCRIPTION**

This appendix documents the calculations used in designing the machinery ventilation and passenger and crew space HVAC systems. These calculations establish minimum ventilation and cooling loads and identify appropriate duct sizes, trunk sizes, and fan and heat pump ratings.

# 2 PROCEDURE

Calculations are presented in the following sequence:

- Passenger Space cooling loads and exhaust fan sizing
- Pilothouse cooling load
- Engine Room ventilation and supply fan sizing
- Jet Room ventilation and exhaust fan sizing

#### **3** GIVEN AND ASSUMED PARAMETERS

• The following environmental conditions were used to determine the HVAC loads:

Environmental Condition	
Cooling Outside Air Dry Bulb Temperature (F)	88
Cooling Outside Air Relative Humidity (%)	75
Cooling Sea Water Temperature (F)	85
Air Conditioned Spaces Temperature (F)	72
Air Conditioned Spaces Humidity (%)	55
Machinery Space Temperature (F)	115
Heating Outside Air Temperature	40
Heating Accommodations Indoor Air Temperature	68
Heating Machinery Space Indoor Air Temperature	50

- Passenger Space and Pilothouse will be served by mini-split heat pump units. Mini-split units will provide cooling and heating to each space.
- Machinery Spaces will not be supplied with any auxiliary heating.
- Compartment areas and volumes have been estimated based upon arrangements, [1].
- The outside air requirement for the Passenger Space was determined using ASHRAE 62.1 Ventilation for Acceptable Indoor Air Quality, [2].
- Passenger Space window glass solar factor (GSF) was modified for geographic location, and an assumed window film per ASHRAE fundamentals in accordance with the RLF method of Chapter 17.

- The Engine Rooms will be provided with mechanical supply and natural exhaust.
- The Jet Rooms will be provided with natural supply and mechanical exhaust.
- All other below deck spaces are provided with natural supply and exhaust.
- Engine Room ventilation is calculated assuming two propulsion engines, Caterpillar C18's rated for 800 HP at 2100 RPM and one generator, Northern Lights M40C3 rated for 40 kW. Heat rejection and air requirements at 100% MCR are tabulated below, [3]
   [4].

Engine Room Equipment Loads	
Propulsion Engine Heat Rejection (btu/min)	1815
Propulsion Engine Consumption Air (cfm)	1856
Generator Engine Cooling Air Required (cfm)	805
Generator Engine Consumption Air (cfm)	114

- Engine Room exhaust air is based upon supply air minus the consumption air of two engines running at 100% MCR.
- Engine Room supply fans have variable frequency drive motors that determine speed based upon a positively pressurized engine room.

# 4 FORMULAS

(not used)

# 5 CALCULATIONS

#### 5.1 Passenger Space Cooling Loads and Exhaust Fan Sizing

Based upon the attached cooling load calculations, the estimated total cooling load for the Passenger Space is approximately 120,000 btu/hr or 10 tons of cooling. The passenger space will be served by four equally sized mini split heat units, each sized for 3.0 tons of cooling. This selection will provide margin and redundancy.

The Passenger Space will be served by an exhaust fan located in the overhead at the aft end of the accommodations. At minimum this fan shall exhaust approximately 600 cfm of air at an estimated static pressure of 1.3 inches H2O.

# 5.2 Pilothouse Cooling Load

Based upon the attached cooling load calculations, the estimated total cooling load for the Pilothouse is approximately 36,000 btu/hr or 3.0 tons of cooling. The Pilothouse will be served by two equally sized mini split heat units, each sized for 2 tons of cooling. This selection will provide margin and redundancy.

#### 5.3 Engine Room Ventilation and Supply Fan Sizing

Based upon the attached calculations a ventilation rate of 10,400 cfm is required to provide cooling and combustion air to the Engine Rooms.

One fan, providing 10,400 cfm, will supply air the each Engine Room. The calculated static pressure is 0.7 inches H2O.

#### 5.4 Jet Room Ventilation and Exhaust Fan Sizing

Based upon the attached calculations a minimum ventilation rate of 157 cfm is required to provide 10 air changes per hour in the Jet Rooms.

One fan, providing 200 cfm, will supply air the each Jet Room. The calculated static pressure is 1.5 inches H2O.

#### REFERENCES

[1] Elliott Bay Design Group, "Profiles and Arrangements," 16109-003-101, Seattle, WA.

[2] ASHRAE, "Standard 62.1-2010 Ventilaton for Acceptable Indoor Air Quality," 2010.

[3] Caterpillar, "Performance Data [EM0270]," 11/10/2016.

[4] Mitsubishi, "ISM Toyota Mistubishi Marine Genset Specs," 2/2016.

Passenger Space				Deck Area: 940 ft <sup>2</sup>						Volume:			7050 ft <sup>3</sup>		
SI		Н	leight:	7.5	ft										
Lighting Load Calculation	n					-									
Description							Area (ff	2)	I.C. (Btu/h	r/ff <sup>2)</sup>		as (btuh)		at (btuh)	
Type of Lighting							I fieu (it.	940	LC, (Duri	1/10	7	6 580		6 580	
								,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,			· · · · · · · · · · · · · · · · · · ·	0,500		0,500	
										Links	u a Tatala	6 5 90		6 5 9 0	
		_		_				_	_	Lignu	ng Totais:	0,380		0,380	
Equipment Load Calculti	lon			(1 + 1)	1.0					¥ Y	<b>T</b>				
Description				qs (btuh)	ql (b	tuh)		Q	lty	Use	Factor	q <sub>s</sub> (btuh)	q <sub>l</sub> (btuh)	q <sub>t</sub> (btuh)	
Coffee Maker (commercial)				6,500	2,0	00		(	0		1				
Electric motor, (5 HP x 2545	/ .87)			14,626				(	0		0.5				
									Fe	uuinme	ent Totals	0	0	0	
Demonstral L and Colorditi										царик	Int Totals.	0	0	0	
Personnel Load Calculut	on Candar	<b>T</b>	_	(1, 1)			_			7		(1 × 1)		(1 + 1)	
Description	Gender	Туре		q <sub>s</sub> (btuh)	q <sub>l</sub> (b	tuh)				ount		q <sub>s</sub> (btuh)	q <sub>l</sub> (btuh)	q <sub>t</sub> (btuh)	
SEATED AT REST	male	1-P1		240		160				0					
SEATED AT REST	mixed	1-P2		210		140				100		21,000	14,000	35,000	
									Р	erson	nel Totals:	21000	14000	35000	
Ventilation Requirement	ts														
Туре	D	escription		Rate	Ur	nit		Oty				OA (cfm)		EX (cfm)	
People Outdoor Air Rate	Public A	Assembly		5	cfm/pe	erson		100	people			500			
Area Outdoor Air Rate	Public A	Assembly		0.06	cfm/so	ıft		940	<u>н</u> <sup>3</sup>			56			
						1			n		*****				
												556			
			11.		1	г	40	<sup>0</sup> E		Cert	0.4.1	350	00	<sup>0</sup> E	
			пе	Looting Unsic	le Air	Tomp	40	°F		001	ng Outsia	e Air Temp	88 72	°F	
Heating and Cooling Log	d Calci	lation	1	leading misic		Iemp H	leating	1				ing Seaso	n 72	1	
Description	Load	Insul		$Area (ft^2)$	т	AT	U or	a (btub)	T (°F)	ΔT	Uor	a (btub)	n (btub)	a (btub)	
Description	Kev	Type		Alea (It)	(°F)		GSF	q <sub>w</sub> (otur)	-(-)		GSF	$q_s$ (bitall)	qi (oturi)	q <sub>t</sub> (btuil)	
Exterior - Weather (Solar)	Over	090-D1	¢↓	812.0	40	28	0.238	5,411	123	51	0.274	11,347		11,347	
Pilot House	Over	090-D4	I↓I	175.0	68	0	0.219		72	0	0.243		0.00.0000000000000000000000000000000000		
Void Space	Belw	090-U4	I↑I	620.0	40	28	0.260	4,514	88	16	0.282	2,797		2,797	
Exterior - Weather	Belw	090-U2	W↑I	320.0	40	28	0.293	2,625	88	16	0.278	1,423		1,423	
Exterior - Weather (Solar)	Fwd	090-H1	☆↔	148.0	40	28	0.259	1,073	108	36	0.287	1,529		1,529	
Exterior - Weather	Fwd	090-H2	W↔I	148.0	40	28	0.259	1,073	88	16	0.260	616		616	
Exterior - Windows (Shaded)	Fwd	001-H2	W↔I	37.0	40	28	1.130	1,171	88	16	1.130	669		669	
Exterior - Windows (Solar)	Fwd	001-H1	-Q↔	37.0	40	28	1.130	1,171	108	36	75	2,775		2,775	
Exterior - Weather	Aft	090-H2	w↔ı	234.0	40	28	0.259	1,697	88	16	0.260	973		973	
Exterior - Weather (Solar)	Port	090-HI	$\chi \leftrightarrow$	217.0	40	28	0.259	1,5/4	108	36	0.287	2,242		2,242	
Exterior Windows (Solar)	Sthd	001-112	W↔I	90.0	40	20	1.130	2,040	100	 	1 1 2 0	0,730		0,730	
Exterior - Weather	Sthd	090-H2	W↔I	217.0	40	20 28	0.250	2,040	00 88	16	0.260	903		903	
	JUU	0,0-112		217.0	υ	20	0.237	1,374		10	0.200	,05		,03	
LIGHTS	Lght											6.580		6.580	
EQUIPMENT	Eqpt											-,2 50		-,2 30	
PERSONNEL	Pers											21,000	14,000	35,000	
Ventilation	OA								88	16		9,258	35,208	44,466	
						Space	e Totals:	27,578			Totals:	70,490	49,208	119,698	

#### Passenger Space Exhaust Fan Total Pressure Calculation

Input	Variables
-------	-----------

Supply Air Temperature $(T_{IN}) =$	88 °F	
Humidity Ratio	0.0217 lb/lb dry air	
Air In Specific Volume (r <sub>IN</sub> ) =	14.29 ft <sup>3</sup> / lb dry air	
Supply air specific weight	0.070 lb/cu ft	
Supply air viscosity	3.89E-07 lb-s/sq ft <sup>2</sup>	
Supply air density	0.0022 slugs/cu ft	
Max Temperature (T <sub>OUT</sub> ) =	90.0 °F	
Air out Specific Volume (r <sub>OUT</sub> ) =	14.34 ft <sup>3</sup> / lb dry air	
Exhaust air specific weight	0.070 lb/cu ft	
Exhaust air viscosity	4.02E-07 lb-s/sq ft2	
Exhaust air density	0.0022 eluge/cu.ft	
Exhaust an density	0.0022 31093/00 10	

Description	height	width	h/w	eqiv	hyd diam	area	length	qty	q	v	Re	f	к	h∟
	(in)	(in)		dia (in)	(in)	(sq ft)	(ft)		(cfm)	(ft/min)				(ft)
upply Ducting														
Inlet Grill, 45 deg taper	6	6	-		6.00	0.20		1	200	1019	4.74E+04	0.024	0.100	0.45
Elbow, R/D = 1.5			-	-	6.00	0.20		1	200	1019	4.74E+04	0.024	0.330	1.48
Round Ducting			-	-	6.00	0.20	12	1	200	1019	4.74E+04	0.024	0.586	2.62
Tee, branch			-	-	4.00	0.09		1	100	1146	3.55E+04	0.027	0.500	2.83
Duct			-	-	4.00	0.09	8	1	100	1146	3.55E+04	0.027	0.638	3.61
Diffuser, L/D = 3	10	10			10.00	0.55		1	100	183	1.42E+04	0.030	0.200	0.03
Tee, branch					4.00	0.09		1	100	1146	3.55E+04	0.000	0.500	2.83
Round Ducting					4.00	0.09	4	1	100	1146	3.55E+04	0.027	0.319	1.81
Elbow					4.00	0.09		1	100	1146	3.55E+04	0.027	0.330	1.87
Diffuser, L/D = 3					10.00	0.55		1	100	183	1.42E+04	0.030	0.200	0.03
				-							Seg	ment total	pressure	17.56

Description	height	width	h/w		hyd diam	area	length	qty	q	v	Re	f	к	hL
	(in)	(in)			(in)	(sq ft)	(ft)		(cfm)	(ft/min)				(ft)
xhaust Vent														
Exhaust Grill, 45 deg Taper, 50% open	12.00	12.00	1.00	-	12.00	0.50		1	400	800	7.19E+04	0.021	0.100	0.28
Damper, D/Do = .9, 50 Deg					8.00	0.35		1	400	1146	6.87E+04	0.022	9.600	54.37
Ducting					8.00	0.35	12	1	400	1146	6.87E+04	0.022	0.404	2.29
Wye, Converging, 45 deg, main					6.00	0.20		1	500	2546	1.14E+05	0.022	0.130	3.64
Duct					6.00	0.20	8	1	500	2546	1.14E+05	0.022	0.352	9.84
Wye, Converging, 45 deg, main					6.00	0.20		1	600	3056	1.37E+05	0.022	0.130	5.24
Duct					6.00	0.20	4	1	600	3056	1.37E+05	0.022	0.173	6.97
Fan					6.00	0.20		1	600	3056	1.37E+05	0.022	0.000	0.00
Louver	10.00	10.00			10.00	0.52		1	600	1152	8.63E+04	0.021	3.600	20.61
								-		-	Seg	ment tota	pressure	103.23

			FT	in H2O
supp	ly air total	pressure	17.56	0.236
exhau	st air total	pressure	103.23	1.389
		Total	120.79	1.626
	15% des	ign margin	138.90	1.869

Exhaust Fan Static Pressure	
Fan Dia (in)	6.00
Fan area (ft2)	0.20
flowrate (cfm)	600
velocity (fpm)	3056
fan velocity pressure	0.5411
Static Pressure for fan selection (in H20)	1.328

Pilothouse					Deck	Area:	175	ft <sup>2</sup>			Vo	lume:	1225	ft <sup>3</sup>
SI	pace No:				ŀ	leight:	7	ft						
Lighting Load Calculation	n													
Description							Area (ff	2)	LC (Btu/h	r/ft <sup>2)</sup>		as (btuh)		at (btuh)
LED lighting							r nou (m	175	20, (Davi	.,	7	1.225		1.225
								1.0				1,220		1,220
	1							1		Light	ng Totolo	1 225		1 225
										Lignu	ng Totais:	1,223		1,223
Equipment Load Calculti	on	_												
Description				qs (btuh)	ql (t	otuh)		Q	ty	Use	Factor	q <sub>s</sub> (btuh)	q <sub>l</sub> (btuh)	q <sub>t</sub> (btuh)
Misc Electronics, (5 HP x 254	5 / .87)			14,626					1		0.5	7,313		7,313
										••••••••••				
									Ec	Juipme	ent Totals:	7313	0	7313
Personnel Load Calcultion	n													
Description	Gender	Туре		q <sub>s</sub> (btuh)	q <sub>l</sub> (t	otuh)			(	Count		q <sub>s</sub> (btuh)	q <sub>l</sub> (btuh)	q <sub>t</sub> (btuh)
SEATED AT REST	male	1-P1		240		160				3		720	480	1,200
SEATED AT REST	mixed	1-P2		210		140				0				
									Р	ercom	nel Totale	720	480	1200
X7									1	cison	ici iotais.	720	400	1200
ventilation Requirement	ts							-					-	
Туре	D	escription		Rate	U	nit		Qty				OA (cfm)		EX (cfm)
By Occupancy	Low Oc	cupancy		15	cfm/p	erson		3	people			45		
Rate of Change	AC, Pilo	ot House		1	ach			1225	ft <sup>3</sup>			20		
Sanitary Fixtures			*****	50	cfm/fi	xture		0	fixture					
												45		
			Hea	ting Outside	Air T	`emp	40	°E		Cool	ng Outsid	e Air Temp	88	°F
			He	ating Inside	Air Te	emp	68	°F		(	Cooling De	esign Temp:	72	°F
Heating and Cooling Loa	d Calcu	lation		d		I	Heating				Cool	ing Seaso	n	
Description	Load	Insul	1	Area $(ft^2)$	Т	ΔΤ	U or	a <sub>w</sub> (btuh)	T (°F)	ΔT	U or	a. (btuh)	a1 (btuh)	g, (btuh)
*	Key	Туре		· I cu (ii )	(°F)		GSF	Jw ( a comp			GSF	13 ( )		
Pilot House Top	Over	090-D1	☆ţ	150.0	40	28	0.238	1,000	123	51	0.274	2,096		2,096
Passenger Space	Belw	090-U4	I↑I	155.0	68	0	0.260		72	0	0.282			
Exterior - Weather (Solar)	Fwd	090-H1	₩↔	104.0	40	28	0.259	754	108	36	0.287	1,075		1,075
Exterior - Weather	Fwd	090-H2	W↔I	0.0	40	28	0.259		88	16	0.260			
Exterior - Windows (Solar)	Fwd	001-H1	☆↔	92.0	40	28	1.130	2,911	108	36	160	14,720		14,720
Exterior - Windows (Shaded)	Aft	001-H2	W↔I	24.0	40	28	1.130	759	88	16	1.130	434		434
Exterior - Weather	Aft	090-H2	W↔I	72.0	40	28	0.259	522	88	16	0.260	300		300
Exterior - Weather (Solar)	Port	090-H1	-Ω↔	28.0	40	28	0.259	203	108	36	0.287	289		289
Exterior - Weather	Port	090-H2	W↔I	28.0	40	28	0.259	203	88	16	0.260	116		116
Exterior - Windows (Solar)	Port	001-H1	Ω↔ WI	16.5	40	28	1.130	522	108	36	160	2,640		2,640
Exterior - Windows (Shaded)	Port	001-H2	W ↔1	16.5	40	28	1.130	522	88	16	1.130	298		298
Exterior - Windows (Snaded)	StDd	001-H2	W	55.0	40	28	1.130	1,044	88	10	1.130	297		297
Exterior - weather	SIDO	090-H2		56.0	40	28	0.239	406	88	10	0.260	233		233
LIGHTS	I oht											1 225		1 225
FOLIPMENT	Fapt											7 313		7 313
PERSONNEL	Pers											720	480	1 200
Ventilation	OA								88	16		749	2.848	3.596
						Spac	e Totals:	8,847			Totals:	32,805	3,328	36,132

# **Engine Room Ventilation**

#### Approach

The minimum required airflow to the Engine Room is calculated based on i) airflow necessary to dissipate heat given off by running equipment, and ii) minimum airflow of 6 air change per hour into the space.

	Equipment Loads	
Main engines Heat Rejection, qe =	1,815.00 btu/min	
Main engines Consumption Air, Qe =	1,856.20 cfm	
Number of Engines Operating, Ne =	2.00	
Generator Cooling Air, $Vg =$	805.00 cfm	
Generator Consumption Air, $Qg =$	114.00 cfm	
Number of Engines Operating, $Ng = $	1.00	
	Inlet Air Conditions	
Summer Air In Temperature (TIN) =	88.00 °F	
Humidity Ratio	0.022 lb/lb dry air	
Air In Enthalpy (hIN) =	45.03 Btu / lb	
Air In Specific Volume (rIN) =	14.29 ft <sup>3</sup> / lb dry air	
	Exhaust Air Conditions	
Max Temperature (TOUT) =	<u>115.00</u> °F	
Air Out Enthalpy (hOUT) =	51.77 Btu / lb	
Air out Specific Volume (rOUT) =	$\frac{14.99}{ft^3}$ / lb dry air	
	Other Givens	
Volume of Space $(V) =$	$1.900 ft^3$	
Minutes per air change $(MA) =$	10.00 min	
Calcula	ated Airflow based on Total He	at Loads
Total Heat Rejection (Qe) =	3630 Btu / min	
D Enthalpy (Dh) =	6.74 Btu / lb	Dh = hOUT - hIN
Required CFM (Heat Load) =	8500 cfm	$CFM = (Qe / Dh \ x \ rIN) + Vg$
	Calculated Exhaust Airflow	
cooling air (V)=	8,500 cfm	(maximum of required airflows)
inlet air specific volume =	14.29 <i>ft3/lb</i>	
exhaust air specific volume =	14.99 ft3/lb	
expansion =	4.93%	
exhaust air =	8,919 cfm	$CFM \equiv V / rIN + rOUT$
	Results	
cooling air =	8,500 cfm	(maximum of required airflows)
consumption air =	3,826 cfm	-
total intake air =	10,413 cfm	(50% combustion air from cooling air)
total exhaust air =	6,701 cfm	

# Engine Room Total Pressure Calculation Input Variables

Supply Air Temperature (T <sub>IN</sub> ) =	88	°F
Humidity Ratio	0.0217	lb/lb dry air
Air In Specific Volume (r <sub>IN</sub> ) =	14.29	ft3 / lb dry air
Supply air specific weight	0.070	lb/cu ft
Supply air viscosity	3.89E-07	lb-s/sq ft <sup>2</sup>
Supply air density	0.0022	slugs/cu ft
Max Temperature (T <sub>OUT</sub> ) =	115.0	°F
Air out Specific Volume (r <sub>OUT</sub> ) =	14.99	ft³ / lb dry air
Exhaust air specific weight	0.067	lb/cu ft
Exhaust air viscosity	4.02E-07	lb-s/sq ft <sup>2</sup>
Exhaust air density	0.0021	slugs/cu ft
Supply air flow rate	10400	cfm
Euclassia dave ante		6 / J

uppiy	all	liow	Iale	10400	CII
haust	air	flow	rate	6600	ft/r

Description	height	width	h/w	eqiv	hyd diam	area	length	qty	q	v	Re	f	к	hL
	(in)	(in)		dia (in)	(in)	(sq ft)	(ft)		(cfm)	(ft/min)				(ft)
Supply Ducting								_						
Inlet Demister	40	30	1.33	36.75	34.29	8.33		1	10400	1248	3.32E+05	0.016	5.500	36.95
Round Fabricated Fire Damper			-	-	30.00	4.91		1	10400	2119	4.93E+05	0.015	0.100	1.94
Fan			-	-	24.00	3.14		1	10400	3310	6.16E+05	0.016	0.000	0.00
Flexible Duct / Round Duct			-	-	32.00	5.59	0.50	1	10400	1862	4.62E+05	0.015	0.003	0.04
Discharge Aft to Gen, R/D = 1.5, 45 deg			-	-	32.00	5.59		1	10400	1862	4.62E+05	0.015	1.200	17.95
Screen (wire mesh)			-	-	32.00	5.59		1	10400	1862	4.62E+05	0.015	0.500	7.48
											Seg	ment total	pressure	64.35
Description	height	width	h/w		hyd diam	area	length	qty	q	v	Re	f	к	hL
	(in)	(in)			(in)	(sq ft)	(ft)		(cfm)	(ft/min)				(ft)
Exhaust Vent														
Damper	27.00	20.00	1.35		22.98	3.75		1	6600	1760	2.90E+05	0.017	0.370	4.94
Inlet	27.00	20.00	1.35		22.98	3.75		1	6600	1760	2.90E+05	0.017	0.500	6.68
Rectangular ducting	40.00	28.00	1.43	-	32.94	7.78	10	1	6600	849	2.00E+05	0.017	0.062	0.19
Exhaust Louver with insect screen	42	42	1.00	-	42.00	9.19		1	6600	718	2.16E+05	0.016	3.600	8.01
								-		-	Seg	ment total	pressure	19.83

		FT	in H2O
supply air total p	ressure	64.35	0.866
exhaust air total p	ressure	19.83	0.267
	Total	84.18	1.133
 15% desig	n margin	96.81	1.303

Supply Fan Static Pressure	
Fan Dia (in)	24.00
Fan area (ft2)	3.14
flowrate (cfm)	10400
velocity (fpm)	3310
fan velocity pressure	0.6074
Static Pressure for fan selection (in H20)	0.696

# Jet Room Ventilation

	Approach	
The minimum required airflow to the Jet Room	m is calculated based on mi	nimum airflow of 10 air change per hour.
	Inlet Air Conditions	
Summer Air In Temperature (TIN) =	88.00 °F	
Humidity Ratio	0.022 lb/lb dry air	
Air In Enthalpy (hIN) =	45.03 Btu / lb	
Air In Specific Volume (rIN) =	14.29 ft <sup>3</sup> / lb dry air	
	Exhaust Air Conditions	
Max Temperature (TOUT) =	<u>90.00</u> °F	
Air Out Enthalpy (hOUT) =	45.53 Btu / lb	
Air out Specific Volume (rOUT) =	14.34 ft³ / lb dry air	
	Other Givens	
Volume of Space $(V) =$	940 $ft^{3}$	
Minutes per air change (MA) =	6.00 min	10 ACH
Calculated A	irflow based on minimum air e	xchanges:
Volume of Space $(V) =$	940 $ft^3$	
Air exchanges / min (AC)=	6 min/AC	
Required CFM(Air Exchange) =	157 cfm	CFM = V/MA

#### Jet Room Total Pressure Calculation Input Variables

Supply Air Temperature (T <sub>IN</sub> ) =	88	°F
Humidity Ratio	0.0217	lb/lb dry air
Air In Specific Volume (r <sub>IN</sub> ) =	14.29	ft <sup>3</sup> / Ib dry air
Supply air specific weight	0.070	lb/cu ft
Supply air viscosity	3.89E-07	lb-s/sq ft <sup>2</sup>
Supply air density	0.0022	slugs/cu ft
Max Temperature (T <sub>OUT</sub> ) =	90.0	°F
Max Temperature (T <sub>OUT</sub> ) = Air out Specific Volume (r <sub>OUT</sub> ) =	90.0 14.34	°F ft³ / lb dry air
Max Temperature (T <sub>OUT</sub> ) = Air out Specific Volume (r <sub>OUT</sub> ) = Exhaust air specific weight	90.0 14.34 0.070	°F ft³ / lb dry air lb/cu ft
Max Temperature (T <sub>OUT</sub> ) = Air out Specific Volume (r <sub>OUT</sub> ) = Exhaust air specific weight Exhaust air viscosity	90.0 14.34 0.070 4.02E-07	°F ft³ / lb dry air lb/cu ft lb-s/sq ft <sup>2</sup>
Max Temperature (T <sub>OUT</sub> ) = Air out Specific Volume (r <sub>OUT</sub> ) = Exhaust air specific weight Exhaust air viscosity Exhaust air density	90.0 14.34 0.070 4.02E-07 0.0022	°F ft <sup>3</sup> / lb dry air lb/cu ft lb-s/sq ft <sup>2</sup> slugs/cu ft
Max Temperature (T <sub>OUT</sub> ) = Air out Specific Volume (r <sub>OUT</sub> ) = Exhaust air specific weight Exhaust air viscosity Exhaust air density	90.0 14.34 0.070 4.02E-07 0.0022	°F ft <sup>3</sup> / Ib dry air Ib/cu ft Ib-s/sq ft <sup>2</sup> slugs/cu ft

200 ft/min

Exhaust air flow rate

Description	height	width	h/w	eqiv	hyd diam	area	length	qty	q	v	Re	f	к	hL
	(in)	(in)		dia (in)	(in)	(sq ft)	(ft)		(cfm)	(ft/min)				(ft)
Exhaust Ducting										-				
Gooseneck inlet with screen			-	-	4.03	0.09		1	200	2258	7.05E+04	0.024	1.400	30.78
4" Sch 40 pipe			-	-	4.03	0.09	5	1	200	2258	7.05E+04	0.024	0.364	8.01
Fan			-	-	4.00	0.09		1	200	2292	7.11E+04	0.024	0.000	0.00
Sudden Expansion, fan outlet			-	-	4.03	0.09		1	200	2258	7.05E+04	0.024	0.510	11.21
Screen			-	-	4.03	0.09		1	200	2258	7.05E+04	0.024	0.240	5.28
											Seg	ment total	pressure	55.29
Description	height	width	h/w		hyd diam	area	length	qty	q	v	Re	f	к	hL
	(in)	(in)			(in)	(sq ft)	(ft)		(cfm)	(ft/min)				(ft)
Supply Vent														
Inlet - Projecting			-	-	4.03	0.09		1	200	2258	6.82E+04	0.025	0.550	12.09
4" Sch 40 pipe			-	-	4.03	0.09	5	1	200	2258	6.82E+04	0.025	0.366	8.04
Gooseneck outlet with screen			-	-	4.03	0.09		1	200	2258	6.82E+04	0.025	2.000	43.98
								-			Seg	ment total	pressure	64.11

		FT	in H2O
exhaust air total	pressure	55.29	0.744
supply air total	pressure	64.11	0.863
	Total	119.40	1.607
15% desi	gn margin	137.31	1.848

Supply Fan Static Pressure	
Fan Dia (in)	4.00
Fan area (ft2)	0.09
flowrate (cfm)	200
velocity (fpm)	2292
fan velocity pressure	0.3043
Static Pressure for fan selection (in H20)	1.544

# **Appendix B**

Fuel Oil System

# **1 DESCRIPTION**

This appendix documents the first principles calculations used in designing the fuel oil system. These calculations are used to identify steady state frictional losses throughout the piping system and to validate system design.

# 2 PROCEDURE

Calculations are presented in the following sequence:

- Pipe size calculations
- Engine fuel pump suction pressure calculations

Frictional losses through the piping system are calculated by constructing a model using PIPE-FLO Professional software with the Darcy Weisbach method applied.

# **3 GIVEN AND ASSUMED PARAMETERS**

- Maximum fuel flow rate to each main engine is 3.53 gpm, from [1].
- Maximum fuel flow rate to each generator is 0.16 gpm, from [2].
- Piping system lengths, routing, fittings, etc. are estimated based on the Profiles and Arrangements, and Fuel Oil Diagram [3] [4].
- Listed main engine fuel system design constraints [1]:

**Table 1: Main Engine Fuel System Design Constraints** 

Engine	Maximum
Allowable supply line restriction to main engine	4.37 psi
Allowable return line restriction to main engine	3.93 psi

- Pressure drop across the Racor 791000MAVM triplex fuel filter for a flowrate of 3.53 gpm is 1 psi, from [5].
- Pressure drop across the Racor 1000MAM fuel filter is for a flowrate of .016 gpm is 0.03 psi, from [6].
- Tank and engine elevations were estimated from [3],all elevations are in reference to the vessel's baseline:

	<b>Elevation Point</b>	Elevation
Fuel tank low fuel level		3.5 feet
Fuel tank high fuel level		7.5 feet
Main Engine fuel inlet		4 feet
Main Engine fuel outlet		5.8 feet
Generator fuel inlet		4.25 feet
Generator fuel outlet		4.8 feet

#### **Table2: Elevations**

#### 4 FORMULAS

(not used)

#### 5 CALCULATIONS

#### 5.1 Pipe Size Calculations

Pipe sizes are based on the nominal velocity limits found in Marine Engineering, Chapter 20, Table 3, [7]. The following table shows the flow rates of fuel occurring in the system, and the resulting pipe/tube sizes.

Dina Sagmant	Flow Rate	Pipe/Tube Size	ID	Design Ve	locity (ft/s)	V
Pipe Segment	gpm	(NPS/0.065 Wall)	in	Nominal	Limit	ft/s
Fill Rate	50	2" Sch 80	1.940	6.96	12.00	5.29
Supply Main (2 me, 1 gen)	7.22	1.5" Tube	1.370	2.34	7.00	1.53
Return main (2 me, 1 gen)	7.22	1.5" Tube	1.370	5.85	12.00	1.53
Main Engine - Supply	3.53	1" Tube	0.870	1.87	7.00	1.86
Generator - Supply	0.16	0.5" Tube	0.370	1.22	7.00	0.46
Main Engine - Return	3.53	1" Tube	0.870	4.66	12.00	1.86
Generator - Return	0.16	0.5" Tube	0.370	3.04	12.00	0.46

#### Table 3: Fuel Oil System Pipe Sizes and Velocities

#### 5.2 Engine Fuel Suction Pressure Calculations

The main engines are supplied with fuel pumps used to draw fuel from fuel tanks. The attached system model confirms that the piping systems are compatible with the engines' fuel supply allowable line restriction requirements. As listed above, the maximum fuel line restriction is 4.37 psi. The attached model shows the calculated pressure loss to be 1.95 psi.

Due to the very low fuel flow rate of the generators compared to the fuel filter and tubing size, the calculated pressure loss for the generator fuel suction is 0.85 psi.

#### 5.3 Engine Fuel Return Pressure Calculations

The attached model of the fuel system's return piping confirms that the backpressure at the main engines does not exceed the listed maximum value of 3.93psi. The return line restriction at the main engines was found to be 1.35 psi.

The generators fuel return line restriction was found to be 1.5 psi as shown in the attached model.

#### **6 REFERENCES**

- [1] Caterpillar, "C18 Systems Data," EM0270, 12/19/2016.
- [2] Northern Lights, "ISM Toyota Mitsubishi Marine Genset Specs; Model M944T3," Feb 2016.
- [3] Elliott Bay Design Group, "NCDOT Pedestrian Ferry: Profiles and Arrangements," 16109-003-101-1, Seattle, WA.
- [4] Elliott Bay Design Group, "NCDOT Pedestrian Ferry: Fuel Oil Diagram," 16109-003-261-1, Seattle, WA.
- [5] Parker Racor, "Racor Products Catolog: Marine Fuel Filtration Products: 79/1000MAV".
- [6] Parker Racor, "Racor Products Catolog:Marine Fuel Filtration Products: 1000MA".
- [7] R. L. Harrington, Marine Engineering, Jersey City, NJ: SNAME, 1992.



NCDOT

			LIST NCPUL				
File Name: Fuel Supp Lineup: <design c<br="">Progam Name: PIPE-FLO Version: 15.2.3731</design>	ly pipe ass> Professional 6	Calculation Method Laminar Cutoff Re Max Herations Iteration Tolerance Atmospheric Pressure	11: Darcy-Weisbach 12: 2100 13: 100 14: 7 psi a	Company: Project: by: Date:	EBDG 16109 JHP Wednesday, February 0	08, 2017 09:14 <i>1</i>	W
:	:	ā.	pe Specifications				
Specification Name Valve Table	Naterial Schedule	Absolute Koughness Hazen Williams C Factor	Sizing Griteria	Velocity	Pressure	e	Reynolds Number
ASTM-A-269 .120 Wall standard	SS teel ASTM-A-269 Schedule: 12	6E-05 in 100	0.0	to ft/s	ţ	psi g	fo
ASTM-A-269 .049 Wall standard	SS teel ASTM-A-269 Schedule: 049	6E-05 in 100	0.0	to ft/s	ţo	psig	fo
ASTM-A-269 .083 Wall standard	SS teel ASTM-A-269 Schedule: 083	6E-05 in 100	0.0	to ft/s	ţ	psig	fo
ASTM-A-269 0.065 Wall standard	SSteel ASTM-A-269 Schedule: 065	6E-05 in 100	0.0	to ft/s	to	psi g	to
			Fluid Zones			l	
Fluid Zone Name Table Name	Temperature	Pressure	uid State	Density Viscosity	Vapor Pressure Critical Pressure	N. S.	pecific Heat Ratio (k) Iative Molecular Mass
Fuel 3 Fuel 3 Max	50 °F	0 psig L	-iquid	56.38 lb/ft³ 10.19 cP	0.2171 psia 3199 psia		1 ←
			Pipelines				
Pipeline Name Specification Fluid Zone	Size Inside Diam Length	Inlet Elevation heter Outlet Elevation	Flow Rate Fluid Velocity Reynolds Number	Total Head Loss V&F Head Loss	Inlet Pressure Outlet Pressure	Total dP V&F dP	Pipe Friction Factor V&F Friction Factor V&F Resistance K
<b>Pipe 1</b> ASTM:A-269 0.065 Wall Fuel 3	1.5 in 1.37 in 25 ft Inlet Device: FO Tank	2.5 ft 3.5 ft	7.22 gpm 1.571 ft/s 1477 Outlet Device:	0.4875 ft 0.1233 ft : Node 1	0.3915 psig -0.1909 psig	0.5824 psi 0.04829 psi	0.04333 0.02101 3.21
<b>Pipe 3</b> ASTM-A-269 0.065 Wall Fuel 3	1.5 in 1.37 in 10 代 Inlet Device: Node 1	3.5 ft 3.5 ft	7.06 gpm 1.537 ft/s 1444 Outlet Device:	0.2426 ft 0.1002 ft : Node 2	-0.1909 psig -0.2859 psig	0.095 psi 0.03923 psi	0.04432 0.02101 2.73
<b>Pipe 5</b> ASTM-A-269 0.065 Wall Fuel 3	1 in 0.87 in 15 ft Inlet Device: Node 2	3.5 ft 3.5 ft	3.53 gpm 1.905 ft/s 1137 <b>Outlet Device</b> :	0.9443 ff 0.2874 ff : Racor 79/1000	-0.2859 psig -0.6556 psig	0.3697 psi 0.1125 psi	0.05629 0.02363 5.10
<b>Pipe 6</b> ASTM-A-269 0.065 Wall Fuel 3	1 in 0.87 in 5 ft Inlet Device: Racor 79/10	3.5 ft 4 ft 00	3.53 gpm 1.905 ft/s 1137 Outlet Device:	0.3256 ft 0.1066 ft : ME Aft	-1.636 psig -1.959 psig	0.3232 psi 0.04175 psi	0.05629 0.02363 1.89
<b>Pipe 4</b> ASTM-A-269 0.065 Wall Fuel 3	1 in 0.87 in 10 ft Inlet Device: Node 2	3.5 ft 3.5 ft	3.53 gpm 1.905 ft/s 1137 Outlet Device:	0.6587 ft 0.2208 ft : Racor 79/1000 1	-0.2859 psig -0.5437 psig	0.2579 psi 0.08644 psi	0.05629 0.02363 3.91
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Pipeline Name Specification Fluid Zone		Size Inside Diameter Length	Inlet Elevation Outlet Elevation	Flow Rate Fluid Velocity Reynolds Number	Total Head Loss V&F Head Loss	Inlet Pre Outlet Pr	ssure essure	Total dP V&F dP	Pipe Friction Factor V&F Friction Factor V&F Resistance K
<b>Pipe 7</b> ASTM-A-269 0.065 Wall Fuel 3	Inlet Device:	1 in 0.87 in 5 ft Racor 79/1000 1	3.5 ft 4 ft	3.53 gpm 1.905 ft/s 1137 <b>Outlet Device:</b> N	0.3256 ft 0.1066 ft 1E FWD	-1.524 -1.848	psig psig 0.	0.3232 psi .04175 psi	0.05629 0.02363 1.89
<b>Pipe 2</b> ASTM-A-269 0.065 Wall Fuel 3	Inlet Device:	0.5 in 0.37 in 10 ft Node 1	3.5 ft 3.5 ft	0.16 gpm 0.4774 ft/s 121.2 <b>Outlet Device</b> : F	0.6215 ft 0.01476 ft tacor 1000	-0.1909 -0.4342	psig 5.78	0.2433 psi 30E-03 psi	0.5281 0.03012 4.17
<b>Pipe 8</b> ASTM-A-269 0.065 Wall Fuel 3	Inlet Device:	0.5 in 0.37 in 3 ft Racor 1000	3.5 ft 4.25 ft	0.16 gpm 0.4774 ft/s 121.2 Outlet Device: C Tanks	0.1906 ft 8.535E-03 ft enset	-0.4608 -0.8291	psig 3.34 psig 3.34	0.3682 psi 41E-03 psi	0.5281 0.03012 2.41
Tank Name Fluid Zone	Bottom Elevation Liquid Level	Surface Press Bottom Press	ure Hydraulic G ure	irade Pipeline	Name Penetrat	Connecting ion Height	l Pipelines Pipeline Flo	w Rate Pre	ssure at Penetration
<b>FO Tank</b> Fuel 3	2.5 ft 1 ft	0 psig 0.3915 psig	3.5 Cui	ft ve dP Devices	Pipe 1 0	Ŧ	7.22	шф	0.3915 psi g
Curve dP Device Name Description	Inlet Inlet	Elevation Pressure	Outlet Elevation Outlet Pressure	Hea	dP 1 Loss	Flow Rate			
Racor 79/1000 Racor 79/1000	-0.65	1.5 ft 56 psig	3.5 ft -1.636 psi g	0.98	16 psi 14 ft	3.53 gpm			
Racor 1000 Racor 1000	-0.43	1.5 ft 42 psig	3.5 ft -0.4608 psi g	0.026	17 psi 11 ft	0.16 gpm			
Racor 79/1000 1 Racor 79/1000	-0.54	.5 ft 37 psig	3.5 ft -1.524 psig	0.98 2.51 Nordes	06 psi )4 ft	3.53 gpm			
Node Name			Elevation	Pressure	Hydraulic	Grade			
Node 1			3.5 ft	-0.1909 psi g	2.986	ft			
Node 2		1	3.5 ft F	-0.2859 psi g ow Demands	2.72	ft	1	1	
Flow Demand Name			Elevation	Pressure	Hydraulic	Grade	Flow Rate	Flow Di	rection
ME Aft			4 ft	-1.959 psi g	-1.061 ft			Flow	v out
Me Fwd			4 ft	-1.848 psi g	-0.7753 ft			Flow	v out
Genset			4.25 ft	-0.8291 psi g	2.129 ft			Flow	r out

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List Report

		Bill of	Materials Repo	ort		
File Name: Lineup: Program Name: Version:	Fuel Supply.pipe <design case=""> PIPE-FLO Professional 15.2.37316</design>			Company: Project: by: Date:	EBDG 16109 JHP Wednesday	r, February 08, 2017 09:15 AM
			Pipelines			
Pipeline	Specif	fication	Size	Len	igth	Valves and Fittings
Pipe 1	ASTM	-A-269 0.065 Wall	1.5 in	25	ft	3 x Elbow - Standard 90° 3 x Pipe Bend - r/d 1 (90°) 1 x Ball
Pipe 3	ASTM	-A-269 0.065 Wall	1.5 in	10	ft	2 x Pipe Bend - r/d 1 (90°) 3 x Elbow - Standard 90°
Pipe 5	ASTM	-A-269 0.065 Wall	1 in	15	ft	1 x Ball 4 x Pipe Bend - r/d 1 (90°) 4 x Elbow - Standard 90° 1 x Reducer - Contraction (1 in x 1.5 in -
Pipe 6	ASTM	-A-269 0.065 Wall	1 in	5	ft	4 x Pipe Bend - r/d 1 (90°)
Pipe 4	ASTM	-A-269 0.065 Wall	1 in	10	ft.	3 x Pipe Bend - r/d 1 (90°) 3 x Elbow - Standard 90° 1 x Ball 1 x Reducer - Contraction (1 in x 1.5 in -
Pipe 7	ASTM	-A-269 0.065 Wall	1 in	5	ft	4 x Pipe Bend - r/d 1 (90°)
Pipe 2	ASTM	-A-269 0.065 Wall	0.5 in	10	ft	3 x Pipe Bend - r/d 1 (90°) 2 x Elbow - Standard 90° 1 x Reducer - Contraction (0.5 in x 1.5 in 1 x Ball
Pipe 8	ASTM	-A-269 0.065 Wall	0.5 in	3	ft	4 x Pipe Bend - r/d 1 (90°)
		Pipe	line Material Sum	nmary		
Specification	Material		Size	Total Length	Valve	s & Fittings
ASTM-A-269 0.0	65 Wall SSteel ASTN Schedule: .	M-A-269 065	0.5 in	13.00 ft	1 x B; 2 x Ei 7 x Pi 1 x R;	all bow - Standard 90° pe Bend - r/d 1 (90°) educer - Contraction (0.5 in x 1.5 in - 0 in)
ASTM-A-269 0.0	65 Wall SSteel ASTN Schedule: .	M-A-269 065	1 in	35.00 ft	2 x B; 7 x Ei 15 x F 2 x R;	all bow - Standard 90° ²ipe Bend - r/d 1 (90°) educer - Contraction (1 in x 1.5 in - 0 in)
ASTM-A-269 0.0	65 Wall SSteel AST Schedule: .	M-A-269 065	1.5 in	35.00 ft	1 x B: 6 x El 5 x Pi	all bow - Standard 90° pe Bend - r/d 1 (90°)

PIPE-FLO Professional

Bill of Materials Report

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<b>File Name:</b> Fuel Return.pipe Lineup: <design case=""></design>		Calculation Metho Laminar Cutoff R	<b>d:</b> Darcy-Weisbach <b>e:</b> 2100	Company: Project:	EBDG 16109		
Progam Name: PIPE-FLO Profes Version: 15.2.37316	sional	Max Iteration Iteration Toleranc Atmospheric Pressur	s: 100 se: 0.01 se: 14.7 psia	by: Date:	JHP Wednesday, February	y 08, 2017 09:16 ,	AM
		<u>е</u>	ipe Specifications				
Specification Name	Material	Absolute Roughness	Sizing Criteria		Design	Limits	
Valve Table	Schedule	Hazen Williams C Factor		Velocity	Pressu	ure	Reynolds Number
ASTM-A-269 .120 Wall standard	SSteel ASTM-A-269 Schedule::12	6E-05 in 100	0.0	to ft/s	to	psi g	to
ASTM-A-269 .049 Wall standard	SSteel ASTM-A-269 Schedule: 049	6E-05 in 100	0.0	to ft/s	to	psi g	to
ASTM-A-269 .083 Wall standard	SSteel ASTM-A-269 Schedule: 083	6E-05 in 100	0.0	to ft/s	to	psi g	to
ASTM-A-269 0.065 Wall standard	SSteel ASTM-A-269 Schedule:.065	6E-05 in 100	0.0 Fluid Zones	to ft/s	ţ	psi g	to
Fluid Zone Name Table Name	Temperature	Pressure	uid State	Density Viscosity	Vapor Pressure Critical Pressure	R S	pecific Heat Ratio (k) Ilative Molecular Mass
Fuel 3 Fuel 3 Max	50 °F	0 psi g	Liquid	56.38 lb/ft <sup>3</sup> 10.19 cP	0.2171 psia 3199 psia		←
			Pipelines				
Pipeline Name Specification Fluid Zone	Size Inside Dian Length	Inlet Elevation leter Outlet Elevation	Flow Rate Fluid Velocity Reynolds Number	Total Head Loss V&F Head Loss	Inlet Pressure Outlet Pressure	Total dP V&F dP	Pipe Friction Factor V&F Friction Factor V&F Resistance K
	)						
<b>Pipe 1</b> ASTM-A-269 0.065 Wall Fuel 3	1.5 in 1.37 in 25 ft Inlet Device: Node 1	3.5 ft 2.5 ft	7.22 gpm 1.571 ft/s 1477 Outlet Device	0.4875 ft 0.1233 ft : FO Tank	1.757 psig 1.958 psig	-0.2007 psi 0.04829 psi	0.04333 0.02101 3.21
<b>Pipe 2</b> ASTM-A-269 0.065 Wall Fuel 3	0.5 in 0.37 in 10 ft Inlet Device: Genset	4.8 ft 3.5 ft	0.16 gpm 0.4774 ft/s 121.2 Outlet Device	0.6318 ft 0.02511 ft : Node 1	1.495 psig 1.757 psig	-0.2616 psi 9.832E-03 psi	0.5281 0.03012 7.09
<b>Pipe 4</b> ASTM-A-269 0.065 Wall Fuel 3	1 in 0.87 in 10 ft Inlet Device: ME FWD	5.8 ft 3.5 ft	3.53 gpm 1.905 ft/s 1137 Outlet Device	0.788 ff 0.3501 ff : Node 2	1.26 psig 1.852 psig	-0.592 psi 0.1371 psi	0.05629 0.02363 6.21
Pipe 5		5.8 ft	3.53 gpm	1.074 ft	1.372 psi g	-0.4802 psi	0.05629
AS I M-A-269 U.U65 Wall Fuel 3	0.87 in 15 ft Inlet Device: ME Aft	11 Q.S	1.905 ft/s 1137 Outlet Device	0.4167 п : Node 2	6 isd 2001	U.1632 psi	0.02363 7.39
-		1	1				
<b>Pipe 3</b> ASTM-A-269 0.065 Wall Fuel 3	1.37 in 1.37 in 10 ft	3.5 ft	7.06 gpm 1.537 ft/s 1444	0.1002 ff	1.852 psig 1.757 psig	udd 0.03923 psi isq 23923 psi	0.0 <del>44</del> 32 0.02101 2.73
	Inlet Device: Node 2		Outlet Device	: Node 1			
PIPE-FLO Professional	Lis	t Report		Wednesday, February 08	, 2017 09:16 AM		Page 1

North CAROLINA D. O. T. Pedestrian Ferry

List Report

PIPE-FLO Profi

Tank Name Fluid Zone	Bottom Elevation Liquid Level	Surface Pressure Bottom Pressure	Hydraulic Grade	Pipeline Name	Connectin Penetration Height	g Pipelines Pipeline Flow Rate	Pressure at Penetration
Fo Tank Fuel 3	2.5 ft 5 ft	0 psig 1.958 psig	7.5 ft	Pipe 1	0 ft	7.22 gpm	1.958 psi g
			Nodes				
Node Name			Elevation	Pressure	Hydraulic Grade		
Node 1			3.5 ft	1.757 psi g	7.961 ft		
Node 2			3.5 ft	1.852 psi g	8.18 ft		
			Flow Dema	nds			
Flow Demand Name		ш	levation	Pressure	Hydraulic Grade	Flow Rate Flov	v Direction
ME Aft			5.8 ft	1.372 psi g	9.247 ft		Flow in
ME FWD			5.8 ft	1.26 psig	8.962 ft		Flow in
Genset			4.8 ft	1.495 psig	8.616 ft		Flow in

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PIPE-FLO Professional

List Report

	Bill o	of Materials Rep	port	
File Name: Fuel Return., Lineup: <design cas<br="">Program Name: PIPE-FLO Pr Variation: 15.2.97316</design>	oipe e> ofessional		Company: EB Project: 161 by: JHF	DG 109 P reference: 08, 2017, 00:46, AM
version. 15.2.57310		Pinelines	Date. We	chesuay, February 06, 2017 09.10 AM
Pipeline	Specification	Size	Length	n Valves and Fittings
Pipe 1	ASTM-A-269 0.065 Wall	1.5 in	25 ft	3 x Elbow - Standard 90° 3 x Pipe Bend - r/d 1 (90°) 1 x Ball
Pipe 2	ASTM-A-269 0.065 Wall	0.5 in	10 ft	3 x Pipe Bend - r/d 1 (90°) 2 x Elbow - Standard 90° 1 x Reducer - Contraction (0.5 in x 1.5 in 1 x Swing Check - Angled
Pipe 4	ASTM-A-269 0.065 Wall	1 in	10 ft	3 x Pipe Bend - r/d 1 (90°) 3 x Elbow - Standard 90° 1 x Reducer - Contraction (1 in x 1.5 in - 1 x Swing Check - Angled
Pipe 5	ASTM-A-269 0.065 Wall	1 in	15 ft	4 x Pipe Bend - r/d 1 (90°) 4 x Elbow - Standard 90° 1 x Reducer - Contraction (1 in x 1.5 in - 1 x Swing Check - Angled
Pipe 3	ASTM-A-269 0.065 Wall	1.5 in	10 ft	2 x Pipe Bend - r/d 1 (90°) 3 x Elbow - Standard 90°
	Pip	eline Material Su	mmary	
Specification	Material	Size	Total Length	Valves & Fittings
ASTM-A-269 0.065 Wall	SSteel ASTM-A-269 Schedule: .065	0.5 in	10.00 ft	2 x Elbow - Standard 90° 3 x Pipe Bend - r/d 1 (90°) 1 x Reducer - Contraction (0.5 in x 1.5 in - 0 in) 1 x Swing Check - Angled
ASTM-A-269 0.065 Wall	SSteel ASTM-A-269 Schedule: .065	1 in	25.00 ft	7 x Elbow - Standard 90° 7 x Pipe Bend - r/d 1 (90°) 2 x Reducer - Contraction (1 in x 1.5 in - 0 in) 2 x Swing Check - Angled
ASTM-A-269 0.065 Wall	SSteel ASTM-A-269 Schedule: .065	1.5 in	35.00 ft	1 x Ball 6 x Elbow - Standard 90° 5 x Pipe Bend - r/d 1 (90°)

PIPE-FLO Professional

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# Appendix C

Sea Chests and Seawater Cooling

# **1 DESCRIPTION**

This appendix documents the calculations used in designing the seawater cooling system. These calculations establish minimum sea chest area and seawater suction pipe sizes. Estimated losses through the system piping are not calculated as the system heat exchangers are supplied by the engine manufacturers and all cooling lines discharge into wet exhaust systems designed and provided by others.

## 2 PROCEDURE

Calculations are presented in the following sequence:

- Seawater pipe nominal velocity calculation
- Sea chest cross sectional area

Initial pipe sizes are based on the nominal velocity limits found in [1], Chapter 20, Table 3.

# **3** GIVEN AND ASSUMED PARAMETERS

- Seawater system is to be constructed of sch 40 aluminum pipe.
- System pipe lengths, routing and fittings are estimated based on the Profiles and Arrangements, [2].
- Total area of pipes connected to an individual sea chest is 7.393 square inches based upon one 3 inch sch 40 suction pipe.

# 4 FORMULAS

(not used)

# 5 CALCULATIONS

#### 5.1 Pipe Nominal Velocity Calculation

Pipe sizes are based on the nominal velocity limits found in [1]. Table 1 shows the flows occurring in all branches of the system, and the resulting pipe sizes:

Pipe Segment	Flow Rate	Pipe Size	ID	Design Vel	ocity (ft/s)	V
	gpm	(NPS)	in	Nominal	Limit	ft/s
Main Engine	100	3" Sch 40	3.068	5.25	15.00	4.23
Generator	11.3	1" Sch 40	1.049	3.07	15.00	4.09
Fire Pump	50	2" Sch 40	2.067	4.31	15.00	4.66
Main Engine & Generator	111.3	3" Sch 40	3.068	5.25	15.00	4.70
Jet Oil Cooler	4	1" Hose	1.000	5.00	15.00	1.59

#### Table 1: Nominal Pipe Velocities

# 5.2 Sea Chest Cross Sectional Area

From the calculations below, the minimum cross sectional area for the sea chest is 51.6 square inches.

INPUTS U	nits Used: <u>US</u>	
$A_p = \ \%_{fa} =$	7.39 in2 50%	Total area of pipes taking suction from sea chest Strainer percent free (clear) area
$R_{min=}$ R=	1.5 <u>3</u>	ABS Required strainer clear area to suction area Chosen clear area ratio, not less than $R_{min}$ .
CALCULATION OF S	SEA CHEST CRO	DSS SECTIONAL AREA

$A_{sc} = A$	p*R / % <sub>fa</sub>	Sea chest cross sectional area
$A_{sc} =$	44.36 in2	Sea chest cross sectional area

### REFERENCES

- [1] R. L. Harrington, Marine Engineering, Jersey City, NJ: SNAME, 1992.
- [2] Elliott Bay Design Group, "Profiles and Arrangements," 16109-003-101, Seattle, WA.

# Appendix D

Fire Main

## **1 DESCRIPTION**

This appendix documents the calculations used in designing the fire main system. These calculations establish required pump capacity and quantity in accordance with regulatory requirements. Estimated losses through the system piping are calculated to establish the total dynamic head (TDH) of the fire pump.

# 2 **PROCEDURE**

Calculations are presented in the following sequence:

- Fire main pipe nominal velocity calculation
- Fire pump total dynamic head (TDH)

Minimum fire pump capacity is based upon the requirements found in [1].

Initial pipe sizes are based on the nominal velocity limits found in [2], Chapter 20, Table 3.

Frictional losses through the piping system are calculated by constructing a model using PIPE-FLO Professional software.

# **3 GIVEN AND ASSUMED PARAMETERS**

- Fire main system is to be constructed of sch 40 aluminum piping.
- System pipe lengths, routing and fittings are estimated based on the Profiles and Arrangements, [3].
- In accordance with [1], the fire pump is required to produce 50 gpm with a 60 psig discharge pressure at the outlet of the pump.
- System will be equipped with 1-1/2" UL listed fire hoses and USCG approved nozzles.

# 4 FORMULAS

(not used)

# 5 CALCULATIONS

#### 5.1 Pipe Nominal Velocity Calculation

Pipe sizes are based on the nominal velocity limits found in [2]. Table 1 shows the flows occurring in all branches of the system, and the resulting pipe sizes:

Dina Sagmant	Flow Rate	Pipe Size	ID	Design Ve	locity (ft/s)	V
r ipe Segment	gpm	(NPS)	in	Nominal	Limit	ft/s
Firemain Suction	50	2" Sch 40	2.067	4.31	15.00	4.66
Firemain Discharge	50	2" Sch 40	2.067	7.19	15.00	4.66
Firemain Branch	50	1-1/2" Sch 40	1.610	6.34	15.00	7.67

Table 1: Nominal Pipe Velocities

# 5.2 Fire Pump TDH and NPSH Calculation

From the attached PIPE-FLO model, the fire pump is required to produce about 150 feet TDH at the required flow rate of 51 gpm.

#### REFERENCES

- [1] USCG, "46 CFR, Chapter I, Subchapter T, Part 181 Fire Protection Equipment," 12/8/2016.
- [2] R. L. Harrington, Marine Engineering, Jersey City, NJ: SNAME, 1992.
- [3] Elliott Bay Design Group, "Profiles and Arrangements," 16109-003-101, Seattle, WA.



File Name: 1610 Lineup: Upp Progam Name: PIPE Version: 15.2	09-521revpipe er Deck Statior E-FLO Professi 37316	onal	Calculation Me Laminar Cuto Max Iterat Iteration Toler: Atmospheric Pres.	thod: Darcy-Weisbach ff Re: 2100 tions: 100 ance: 0.01 sure: 14.7 psi a	ບິ	mpany: EBDG Project: 16109.0 by: LGB Date: Friday, I	00 March 03, 2017 09	:55 AM		
				Pipe Specifications						
Specification Name Valve Table		Material Schedule	Absolute Roughnes Hazen Williams C Fac	is Sizing Criteria tor	Veloci	ity	Design Limi Pressure	lts R	teynolds Number	
CuNi Class 200 standard		Copper Nickel MIL-T-16420K Schedule:Class 200	6E-05 in 150	0.0	to	ft/s	ą.	psig	fo	
Al B241 sch 40 standard		Aluminum B241 Schedule:40	6E-05 in 140	0.0	to	ft/s	đ	psi g	fo	
				Fluid Zones						
Fluid Zone Name Table Name		Temperature	Pressure	Fluid State	Density Viscosity	Crit Crit	por Pressure tical Pressure	Sp Rela	ecific Heat Ratio (k) ative Molecular Mass	
Seawater Seawater 3.5% Salinit	<u>م</u>	65°F	0 psig	Liquid	64 lb/ff <sup>2</sup> 1.127 cP	Ó	.2997 psia 3199 psia		- 29	
				Centrifugal Pumps						
Pump Name		Test Speed Operating Speed	Suction Elevation Suction Pressure	Discharge Elevation Discharge Pressure	Total Head dP	Flow Rate Power	Efficiency BEP Efficienc	y NPSH	Ha Design NPSH Hr Margin Ratio	
<b>Sizing Pump 3</b> Fixed Speed		3500 pm 3500 pm	2 ft -0.4013 psig	2 ft 66.17 psig	149.8 ft 66.57 psi	51.23 gpm 4.279 hp	46.2 % 51 %	31.49 9.998	н н	
Company: Ampco Curve: Catalog Type: Z-SERI	Pumps g Pump ES		Size: 1.5x1.25 Diameter: 6 in POR: from -	SS - to -						
<b>Sizing Pump 2</b> Fixed Speed		3500 	2 ft 	2 ft 	1 1	1 1	- 51 %	11		
Company: Ampco Curve: Catalog Type: Z-SERI	Pumps J Pump ES		Size: 1.5x1.25 Diameter: 6 in POR: from -	SS - to -						
				Pipelines						
Pipeline Name Specification Fluid Zone		Size Inside Dia Length	Inlet Elevation Interer Outlet Elevation	on Flow Rate ion Fluid Velocity Reynolds Numbe	Total Head V&F Head I	Loss Inle Loss Outl	et Pressure let Pressure	Total dP V&F dP	Pipe Friction Factor V&F Friction Factor V&F Resistance K	
<b>Pipe 2</b> Al B241 sch 40 Seawater		2 in 2.067 in 35 ft Inlet Device: Sizing Pun	2 ff 16 ff np 3	51.23 gpm 4.899 ft/s 71293 <b>Outlet Devic</b>	3.493 1 2.018 1 <b>e:</b> Node 1	LT LT LT LT LT LT LT LT LT LT LT LT LT L	6.17 psig 8.39 psig	7.775 psi 0.897 psi	0.01946 0.01899 5.41	
<b>Pipe 4</b> Al B241 sch 40 Seawater		1.5 in 1.61 in 30 ft Inlet Device: Node 1	16 ft 16 ft	-  Outlet Devic	e: Node 2	ă	8.39 psig 	11	 9.28	
Pipe 3		1.5 in	16 ft	51.23 apm	8.225 f	1 56	3.39 psi a	6.767 psi	0.01852	
AI B241 sch 40 Seawater		1.61 in 15 ft Inlet Device: Node 1	23 #	8.074 ft/s 91529 Outlet Devic	6.128 t 6.128 t	ي ب	1.63 psig	2.724 psi	0.02018 6.05	
PIPE-FLO Professions	<u>تا</u>	Ľ	ist Report		Friday, Marcl	h 03, 2017 09:55	AM		Page 1	

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				Pipelines				
Pipeline Name Specification Fluid Zone	-	Size nside Diameter Length	Inlet Elevation Outlet Elevation	Flow Rate Fluid Velocity Reynolds Number	Total Head Loss V&F Head Loss	Inlet Pressure Outlet Pressure	Total dP V&F dP	Pipe Friction Factor V&F Friction Factor V&F Resistance K
<b>Pipe 1</b> Al B241 sch 40 Seawater	Inlet Device: 5	2 in 2.067 in 5 ft SEA WATER	0 ff 2 ff	51.23 gpm 4.899 ft/s 71293 Outlet Device: 2	1.117 ft 0.9065 ft " Eafon Model 72	1.556 psig 0.1702 psig	1.385 psi 0.4029 psi	0.01946 0.01899 2.43
Pipe 5 Al B241 sch 40 Seawater	Inlet Device: 2	2 in 2.067 in 2.5 ft 2" Eaton Model 72	2 ff 1	51.23 gpm 4.899 ft/s 71293 Outlet Device: S	0.1053 ft 0 ft (izing Pump 3	-0.3545 psig -0.4013 psig	0.0468 psi 0 psi	0.01946 0.01899 0.00
HOSE AI B241 sch 40 Seawater	Inlet Device: 1	1.5 in 1.61 in 50 ft Vode 2	16 ft 16 ft	  Outlet Device: F	ire Nozzle	1 1	1 1	00.00
<b>spray1</b> Al B241 sch 40 Seawater	Inlet Device: F	1.5 in 1.61 in 0.01 ft ⊐ire Nozzle	16 ft 16 ft				1 1	
HOSE2 AI B241 sch 40 Seawater	Inlet Device: <sup>1</sup>	1.5 in 1.61 in 50 ft Vode 3	23 ff 23 ff	51.23 gpm 8.074 ft/s 91529 <b>Outlet Device:</b> F	6.991 ft 0 ft ire Nozzle1	51.63 psig 48.52 psig	3.107 psi 0 psi	0.01852 0.02018 0.00
<b>spray</b> Al B241 sch 40 Seawater	Inlet Device: F	1.5 in 1.61 in 0.01 ft Fire Nozzle1	23 ff 23 ff	51.23 gpm 8.074 ft/s 91529 <b>Outlet Device</b> : L	1.398E-03 ff 0 ff Jpper Deck Aff Stbd Staf	6.214E-04 psig 0 psig ion	6.214E-04 psi 0 psi	0.01852 0.02018 0.00
Tank Name Fluid Zone	Bottom Elevation Liquid Level	Surface Press Bottom Press	ure Hydraulic G ure	Trade Pipeline	Name Penetratio	Connecting Pipelir n Height Pipelir	ies ie Flow Rate Pr	essure at Penetration
SEA WATER Seawater	0 ff 3.5 ff	0 psig 1.556 psig	3.5	H.	Pipe 1 0 f	1 5	1.23 gpm	1.556 psig
Fire Nozzle 1/2 Fire Nozzle	- ·	6 ft	16 ft 		1 1	1		
Fire Nozzle1 1/2 Fire Nozzle	48.5	3 ft 2 psig	23 ff 6.214E-04 psig	48. 109 Nodes	52 psi 5. .2 ft	1.23 gpm		
Node Name			Elevation	Pressure 58.30 pei d	Hydraulic Gr	ade		
Node 2 Node 2 Node 3				51 63 Disig				
rroue J Pressure Roundary Name			Elevation	sure Boundaries	Hvdraulic Gr	ade	v Rate	
Upper Deck Aft Stbd Station			23 ft	0 psig	21.99 ft	51.23	gpm	
Main Deck Aft port Station1 PIPE-FLO Professional		List Repor	16 ft t	0 psi g	 Friday, March 03, 201	 17 09:55 AM		Page 2

	E	Sill of Materials Re	port	
File Name: 16109- Lineup: Upper I Program Name: PIPE-F Version: 15.2.37	521revpipe Deck Station LO Professional 316		Company: EBD Project: 1610 by: LGB Date: Frid:	0G 09.00 3 ay, March 03, 2017 09:55 AM
		Pipelines		
Pipeline	Specification	Size	Length	Valves and Fittings
Pipe 2	Al B241 sch 40	2 in	35 ft	8 x Elbow - Standard 90° 1 x Butterfly
Pipe 4	AI B241 sch 40	1.5 in	30 ft	1 x Reducer - Contraction (1.5 in x 2 in - 8 x Elbow - Standard 90° 1 x Tee - Flow Thu Branch 1 x Globe - 90°, Plug In Flow Path
Pipe 3	Al B241 sch 40	1.5 in	15 ft	4 x Elbow - Standard 90° 1 x Tee - Flow Thru Run 1 x Reducer - Contraction (1.5 in x 2 in - 1 x Globe - 90°, Plug In Flow Path
Pipe 1	Al B241 sch 40	2 in	5 ft	1 x Gate - Plug Type 4 x Elbow - Standard 90°
Pipe 5	Al B241 sch 40	2 in	2.5 ft	
HOSE	Al B241 sch 40	1.5 in	50 ft	
spray1	Al B241 sch 40	1.5 in	0.01 ft	
HOSE2	Al B241 sch 40	1.5 in	50 ft	
spray	Al B241 sch 40	1.5 in	0.01 ft	
		Pipeline Material Su	immary	
Specification	Material	Size	Total Length	Valves & Fittings
Al B241 sch 40	Aluminum B241 Schedule: 40	1.5 in	1 <b>45.02</b> ft	12 x Elbow - Standard 90° 2 x Globe - 90°, Plug In Flow Path 2 x Reducer - Contraction (1.5 in x 2 in - 0 in) 1 x Tee - Flow Thru Branch 1 x Tee - Flow Thru Run
Al B241 sch 40	Aluminum B241 Schedule: 40	2 in	42.50 ft	1 x Butterfly 12 x Elbow - Standard 90° 1 x Gate - Plug Type

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# Appendix E

Sanitary Drains and Sewage Discharge

### **1 DESCRIPTION**

This appendix documents the calculations used in designing the sewage discharge system. These calculations establish minimum discharge pipe sizes and required pump capacity. Estimated losses through sewage discharge piping are calculated to establish total dynamic head required for the sewage discharge pump.

# 2 PROCEDURE

Calculations are presented in the following sequence:

- Sewage discharge pump capacity calculations
- Sewage discharge pipe nominal velocity calculations
- Sewage pump total dynamic head (TDH) calculation

Initial sewage pump capacity is based on the desire to empty the sewage-holding tank in approximately 5 minutes.

Initial pipe sizes are also based on the nominal velocity limits found in [1], Chapter 20, Table 3.

Frictional losses through the piping system are calculated by constructing a model using PIPE-FLO Professional software.

### **3** GIVEN AND ASSUMED PARAMETERS

- Sewage discharge piping is to be constructed of aluminum.
- System pipe lengths, routing and fittings are estimated based on Profiles and Arrangements [2].
- Shore side facilities are conservatively estimated as 50 feet of 2 inch hose and 200 feet of 2 inch schedule 80 steel piping with a storage tank elevation of 20 feet.

# 4 FORMULAS

(not used)

# 5 CALCULATIONS

#### 5.1 Sewage Discharge Pump Capacity Calculation

The sewage pump capacity is based on the ability to empty the sewage-holding tank in approximately 5 minutes. With a tank of 200 gallon this results in a pump capable of approximately 40 gpm.

#### 5.2 Pipe Nominal Velocity Calculation

Initial pipe sizes are also based on the nominal velocity limits found in [1]. Table 1 shows the flows occurring in all portions of the system, and the resulting pipe sizes:

		•				
Dina Sagmant	Flow Rate	Pipe Size	ID	Design Ve	locity (ft/s)	V
r ipe Segneni	gpm	(NPS)	in	Nominal	Limit	ft/s
Pump Suction	40	3" Sch 80	2.900	5.11	15.00	1.89
Sewage Discharge	40	2" Sch 80	1.940	6.96	15.00	4.23

Table 1: Nominal Pipe Velocities

## 5.3 Sewage Pump TDH Calculation

From the attached PIPE-FLO model, the sewage discharge pump is required to produce about 36 feet TDH at 40 gpm.

### **6 REFERENCES**

[1] R. L. Harrington, Marine Engineering, Jersey City, NJ: SNAME, 1992.

[2] Elliott Bay Design Group, "Profiles and Arrangements," 16109-003-101-1, Seattle, WA.



		l	l	List Report		i		
File Name: 16109-003-528.pit Lineup: <design case=""> Progam Name: PIPE-FLO Profess Version: 15.2.37316</design>	e ional		alculation Metho Laminar Cutoff R Max Iteration teration Toleranc	d: Darcy-Weisbach e: 2100 s: 100 e: 0.01 e: 14.7 osia	Compar Proje	y: EBDG t: 16109 y: JHP e: Wednesday, Janua	ry 18, 2017 12:33 F	Wc
			ā.	ipe Specifications				
Specification Name Valve Table	Material Schedule	Absol Hazen V	ute Roughness Villiams C Factor	Sizing Criteria	Velocity	Desig	jn Limits sure	Reynolds Number
AL B241 sch 80 standard	Aluminum B241 Schedule:80		6E-05 in 140	0.0	to ft/	to	psig	to
Steel A53-B36.10 Sch 80 standard	Steel A53-B36.10 Schedule:80	1.8	00E-03 in 140	0.0	to ft/	s to	psi g	to
				Fluid Zones				
Fluid Zone Name Table Name	Temperatur	re Pres	ssure Fl	uid State	Density Viscosity	Vapor Pressu Critical Pressu	re Ire	Specific Heat Ratio (k) elative Molecular Mass
Water Water	50 °F	0	psi g	Liquid	62.41 lb/ff <sup>3</sup> 1.269 cP	0.1782 psia 3199 psia		1 8
				Sizing Pumps				
Pump Name		Suction Suction	Elevation Di Pressure Di	scharge Elevation scharge Pressure	Total Head F dP	low Rate	NPSHa	
SEWAGE DISCHARGE PUMP		-1.5 0.3256	ft psig	-1.5 ft 15.96 psig Pipelines	36.07 ft 15.64 psi		34.25 ft	
				-				
Pipeline Name Specification Fluid Zone	E	Size side Diameter Length	Inlet Elevation Outlet Elevation	Flow Rate Fluid Velocity Reynolds Number	Total Head Loss V&F Head Loss	Inlet Pressure Outlet Pressure	Total dP V&F dP	Pipe Friction Factor V&F Friction Factor V&F Resistance K
<b>Suction</b> AL B241 sch 80 Water	Inlet Device: SI	3 in 2.9 in 10 ft EWAGE TANK	-1.5 ft -1.5 ft	40 gpm 1.943 ft/s 34379 <b>Outlet Devic</b>	0.2488 ft 0.1934 ft s: SEWAGE DISCHARG	0.4334 psig 0.3256 psig E PUMP	0.1078 psi 0.08384 psi	0.02281 0.01754 3.30
<b>Discharge</b> AL B241 sch 80 Water	Inlet Device: SI	2 in 1.939 in 25 ft EWAGE DISCHAR	-1.5 ff 10 ff GE PUMP	40 gpm 4.346 ft/s 51418 <b>Outlet Devic</b>	2.324 ft 1.376 ft s: VESSEL CONNECTIO	15.96 psig 9.969 psig N	5.991 psi 0.5962 psi	0.02087 0.01928 4.69
Hose Steel A53-B36.10 Sch 80 Water	Inlet Device: V	2 in 1.939 in 50 ft ESSEL CONNECT	10 ft 15 ft ION	40 gpm 4.346 ft/s 51418 <b>Outlet Devic</b>	3.004 ft 0.8491 ft s: TANK ON SHORE	9.969 psig 6.5 psig	3.469 psi 0.368 psi	0.02373 0.01928 2.89
<b>Shore pipe</b> Steel A53-B36.10 Sch 80 Water	Inlet Device: T/	2 in 1.939 in 200 ft ANK ON SHORE	15 ff 20 ff	40 gpm 4.346 ft/s 51418 Outlet Devic	9.997 ft 1.376 ft 9: TANK ON SHORE1	6.5 psig 0 psig	6.5 psi 0.5962 psi	0.02373 0.01928 4.69
Tank Name	Bottom Elevation	Surface Pressu	ire Hydrauli	c Grade		Connecting Pipel	ines	
Fluid Zone	Liquid Level	Bottom Pressu	e	Pipel	ine Name Penetra	iion Height Pipel	ine Flow Rate	Pressure at Penetration
SEWAGE TANK Water	-1.5 ft 1 ft	0 psig 0.4334 psig	Ŷ	.5 ft				
PIPE-FLO Professional		List Report			Wednesday, January	I8, 2017 12:33 PM		Page 1

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Tank Name	Bottom Elevation	Surface Pressure	Hydraulic Grade		Connecti	ng Pipelines	
Fiuld 20ne	ridnia Level	BOTTOM Pressure		Pipeline Name	Penetration Height	грение гюм кате	Pressure at Penetration
SEWAGE TANK Water	-1.5 ft 1 ft	0 psig 0.4334 psig	-0.5 ft				
				Suction	0 ft	40 gpm	0.4334 psi g
			Nodes				
Node Name			Elevation	Pressure	Hydraulic Grade		
VESSEL CONNECTION			10 ft	9.969 psi g	32.71 ft		
TANK ON SHORE			15 ft	6.5 psig	29.7 ft		
			Pressure Bou	ndaries			
Pressure Boundary Name			Elevation	Pressure	Hydraulic Grade	Flow Rate	
TANK ON SHORE1			20 ft	0 psig	19.71 ft	40 gpm	

	Flow Rate	40 gpm
	Hydraulic Grade	19.12 H
Boundaries	Pressure	0 psi g
Pressure	Elevation	20 ft

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	Bill	of Materials Rep	port	
File Name: 16109-0 Lineup: <design Program Name: PIPE-FL Version: 15.2.37</design 	03-528.pipe Case> O Professional 116		Company: EBD Project: 1610 by: JHP Date: Wed	G 19 nesday, January 18, 2017 12:32 PM
		Pipelines		
Pipeline	Specification	Size	Length	Valves and Fittings
Suction	AL B241 sch 80	3 in	10 ft	6 x Elbow - Standard 90° 1 x Gate - Double Disc
Discharge	AL B241 sch 80	2 in	25 ft	8 x Elbow - Standard 90° 1 x Ball
Hose	Steel A53-B36.10 Sch 80	2 in	50 ft	5 x Elbow - Standard 90°
Shore pipe	Steel A53-B36.10 Sch 80	2 in	200 ft	8 x Elbow - Standard 90° 1 x Ball
	P	ipeline Material Su	mmary	
Specification	Material	Size	Total Length	Valves & Fittings
AL B241 sch 80	Aluminum B241 Schedule: 80	2 in	25.00 ft	1 x Ball 8 x Elbow - Standard 90°
AL B241 sch 80	Aluminum B241 Schedule: 80	3 in	10.00 ft	6 x Elbow - Standard 90° 1 x Gate - Double Disc
Steel A53-B36.10 Sch 80	Steel A53-B36.10 Schedule: 80	2 in	250.00 ft	1 x Ball 13 x Elbow - Standard 90°

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# Appendix F

Bilge System

## **1 DESCRIPTION**

This appendix documents the calculations used in designing the bilge system. These calculations establish required pump capacity and quantity in accordance with regulatory requirements. Estimated losses through bilge system piping are calculated to establish the total dynamic head (TDH) for all of the bilge pumps.

# 2 PROCEDURE

Calculations are presented in the following sequence:

- Bilge pump capacity and quantity calculations
- Bilge pipe nominal velocity calculations
- Bilge pump TDH calculation

Bilge pump capacity calculations are based on the requirements found in [1].

Initial pipe sizes are also based on the nominal velocity limits found in [2], Chapter 20, Table 3.

Frictional losses through the piping system are calculated by constructing a model using PIPE-FLO Professional software.

#### **3** GIVEN AND ASSUMED PARAMETERS

- Each water tight compartment will be equipped with a submersible bilge pump. Each Engine Room will be equipped with two submersible bilge pumps. The forward most void will be equipped with a manual pump.
- Bilge system is to be constructed of flexible hose and schedule 80 aluminum pipe.
- Bilge overboard discharges are assumed to be 9 feet above baseline.
- System pipe lengths, routing and fittings are estimated based on the Profiles and Arrangements, [3].

# 4 FORMULAS

(not used)

# 5 CALCULATIONS

#### 5.1 Bilge Pipe Size and Pump Capacity Calculation

From the attached calculations, each demi-hull is required to have a total bilge pump capacity of 30 cubic meters per hour, or 136 gallons per minute. Each pump must have minimum capacity of 7.7 cubic meters per hour, or 34 gallons per minute. However, per [1], the required minimum bilge pump capacity is 8 cubic meters per hour, or 35 gallons per minute.

#### 5.2 Bilge Pipe Nominal Velocity Calculation

Initial pipe sizes are also based on the nominal velocity limits found in [2]. Table 1 shows the flows occurring in all portions of the system, and the resulting pipe sizes:

Dina Sagmant	Flow Rate	Pipe Size	ID	Design Ve	locity (ft/s)	V
r ipe Segment	gpm	(NPS)	in	Nominal	Limit	ft/s
Bilge Hose	35	2" ID Hose	2.000	7.07	15.00	3.48
Bilge Overboard	35	1-1/2" Sch 80	1.500	6.12	15.00	6.19

### Table 1: Nominal Bilge Pipe Velocities

### 5.3 Bilge Pump Total Head and Net Positive Suction Head (NPSH) Calculation

From the attached PIPE-FLO model, each bilge pump is required to produce about 10 feet TDH at the required flow rate of 35 gpm.

#### 6 **REFERENCES**

- Lloyd's Register, "Rules and Regulations for the Classification of Special Service Craft," 2015.
- [2] R. L. Harrington, Marine Engineering, Jersey City, NJ: SNAME, 1992.
- [3] Elliott Bay Design Group, "Profiles and Arrangements," 16109-003-101-0, Seattle, WA.

#### Size of Bilge Main Suction Pipes

Per Lloyd's Register Rules and Regulations for the Classification of Special Service Craft Chapter 15, Section 12, Paragraph 12.3.1

Where a bilge main is fitted in each hull, it's internal diameter dm is not to be less than that required by the following formula:

$$d_m = 1.68\sqrt{L(B+D)} + 25 \ [mm]$$

where

B = breadth D = moulde L = Length	n of a demi-hull in meters ed depth to the watertight d of craft in meters	eck, in meters
B =	9 feet	2.74 meters
D =	11.5 feet	3.51 meters
Γ=	92 feet	28.04 meters
dm=	47.24 mm	1.86 inch

#### Size of Bilge Branch Suctions

Per Lloyd's Register Rules and Regulations for the Classification of Special Service Craft Chapter 15, Section 12, Paragraph 12.3.2

The diameter db of a branch bilge suction pipes is to be not less than that required by the following formula

$$d_b = 2.15\sqrt{C(B+D)} + 12.5 \ [mm]$$

where

C = length of the compartment in meters

Space	C (ft)	C (m)	db (mm)	db (in)
Jet Room	10.00	3.05	29.50	1.16
Engine Room	22.00	6.71	37.71	1.48
Tank Room	32.00	9.75	42.90	1.69
Void 2	12.00	3.66	31.12	1.23

#### **Total Capacity Fixed Submersible Pumps**

Per Lloyd's Register Rules and Regulations for the Classification of Special Service Craft Chapter 15, Section 12, Paragraph 12.4.5

Where fixed submersible bilge pumps are fitted, the total capacity, Qt of the pumps in each hull is to be not less than that required by the following formula:

$$Q_t = \frac{13.8}{10^3} * d_m^2 \ [m^3/hr]$$

Qt =	30.8 m3/hr	136 gpm
		01

100 BP1

#### **Total Capacity Fixed Submersible Pumps**

Per Lloyd's Register Rules and Regulations for the Classification of Special Service Craft Chapter 15, Section 12, Paragraph 12.4.6

The capacity Qn of each submersible pump is to be not less than required by the following formula:

$$Q_n = \frac{Q_t}{(N-1)} \ [m^3/hr]$$

Where

N = numbe r of fixed submersible pumps in each hull Qt = Total Cacity as defined above Qn is in no case to be less than 8 m3/hr

$$N = 5$$
  
 $Qn = 7.7 \text{ m3/hr}$  34 g

34 gpm



File Name: 16109-529,pipe Lineup: Lineup: Cossos Progam Name: PIPE-FLO Professional 		Allo Call	culation Meth minar Cutoff Max Iteratio srcent Tolerar wable Deviat	odd: Darcy-Weisbach Re: 2100 ons: 100 cce: 0.01 ion: 1 %	Com Pro Atmospheric Pres	aany: EBDG ject: 16109 by: LGB Date: Wednesday, sure: 14.7 ps	January 11, 2017 08: i a	55 AM	
				Pipe Specifications	6				
Specification Name Valve Table	Material Schedule	A E	bsolute Roug	ghness Sizing C Factor	l Criteria	Velocity	Design Lin Dressure	iits Revnolde Numhe	.
	onlenne					AEICOLIS			_
Aluminum B241 Sch 80 standard	Aluminum B241 Schedule:80		6E-05 140	in 0.0	Mir Max	tt/s tt/s	psi g psi g		
Hose standard	Sanitary Tubing Schedule:STD		6E-05 100	in 0.0	Mir Max	: ft/s : ft/s	psi g Dsi a		
		l	l	Fluid Zones			-		
Fluid Zone Name Table Name		Temperature Pressure	Fluid Relative N	d State Aolecular Mass	Density Viscosity	Vapor Critica	Pressure Spe I Pressure S	cific Heat Capacity (cp) pecific Heat Ratio (k)	
Sea Water Seawater 3.5% Salinity		65°F 0psig	Lic	tuid 29 String Durage	64 lb/ft³ 1.127 cP	0.299	37 psia 39 psia	1	
Pump Name		Suction El Suction Pr	evation essure	Discharge Elevation Discharge Pressure	Total Head dP	Flow R	late NPS	ł	
Sizing Pump 1		0 fl -1.288E-03 p	isi g	0 ft 4.338 psig	9.764 ft 4.34 psi	35 g	pm 32.39	42	
				Pipelines					
Pipeline Name Specification Fluid Zone	Size Inside Diame Length	Inlet De ter Inlet Elev Outlet D Outlet Ele	vice /ation evice vation	Flow Rate Fluid Velocity Reynolds Number Pipe Friction Factor	Inlet Total Pressure Inlet Static Pressure Inlet Energy Grade Inlet Hydraulic Grade	Total dP Total Head Loss	Outlet Total Pres Outlet Static Pres Outlet Energy Gr Outlet Hydraulic C	sure V&F Friction Fac sure V&F Resistance ade V&F Head Loss rade V&F Head Loss	γ
<b>Pipe 1</b> Hose Sea Water	2 in 1.87 in 14.5 ft	Sizing Pun 0 fl Node 1 9 fl	1 dt	35 gpm 4.089 ft/s 53833 0.02067	4.338 psig 4.223 psig 9.762 ft 9.502 ft	4.316 psi 0.7119 ft	0.02203 psi -0.09343 psi 9.05 ft 8.79 ft	0.01945 0.82 0.09434 psi 0.2123 ft	
<b>Pipe 2</b> Auminum B241 Sch 80 Sea Water	2 in 1.939 in 0.1 ft	Tank 1 0 fl Sizing Pun 0 fl	1 di	35 gpm 3.803 ft/s 51918 0.02083	0 psig -0.09988 psig 0 ft -0.2247 ft	1.288E-03 psi 2.897E-03 ft	-1.288E-03 psi -0.1012 psi -2.897E-03 ft -0.2276 ft	0.01928 0.00 0 ft	
<b>Pipe 3</b> Aluminum B241 Sch 80 Sea Water	1.5 in 1.5 in 0.5 ft	Node 1 9 fi Pressure Bour 9 fi	: Idary 1	35 gpm 6.354 ft/s 67112 0.01975	0.02203 psig -0.2569 psig 9.05 ft 8.422 ft	0.02203 psi 0.04958 ft	0 psi -0.2789 psi 9 ft 8.372 ft	0.02054 0.00 0 psi 0 ft	
				lanks					
Tank Name Fluid Zone	ottom Elevation	Surface Pressure Bottom Pressure	Hydra	ulic Grade	<sup>1</sup> ipeline Name Pene	Connecting tration Height	J Pipelines Pipeline Flow Rate	Pressure at Penetrati	5
Tank 1	0 ft 0 ft	0 psig 0 psig		0 ft	Pipe 2	0	35 gpm	0 psig	

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PIPE-FLO Professional

List Report

	Nodes			
Node Name	Elevation	Pressure	Hydraulic Grade	
Node 1	0 ft 0	.02203 psi g	8.606 ft	
	Pressure Bour	ndaries		
Pressure Boundary Name	Elevation	Pressure	Hydraulic Grade	Flow Rate
Pressure Boundary 1	9 ft	0 psig	8.372 ft	35 gpm

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List Report

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PIPE-FLO Professional

		Bill of N	laterials Repor	t		
File Name:	16109-529.pipe			Company:	EBDG	
Lineup:	<design case=""></design>			Project:	16109	
Program Name:	PIPE-FLO Professional			by:	LGB	
Version:	15.2.37316			Date:	Wednesday, Janua	ary 11, 2017 08:45 AM
			Sizing Pumps			
Sizing Pump Na	me				D	esign Point
Operation					Flow Rate	Total Head
Sizing Pump 1 Flow @ 35 gp	m				35 gpm	<b>9.764</b> ft
			Tanks			
Tank Name						
Tank 1						
			Pipelines			
Pipeline	Specif	cation	Size	Length	Valves and	Fittings
Pipe 1	Hose		2 in	14.5 ft	3 x Elbow -	Long radius, r/d 1.5 (90°)
Pipe 2	Alumin	um B241 Sch 80	2 in	0.1 ft		
Pipe 3	Alumin	um B241 Sch 80	1.5 in	0.5 ft		
		Pipelir	e Material Sumn	nary		
Specification	Material	S	iize T	otal Length	Valves & Fit	tings
Aluminum B241 \$	Sch 80 Aluminum B2 Schedule: 8	241 1 0	.5 in	0.50 ft		
Aluminum B241 :	Sch 80 Aluminum B2 Schedule: 8	241 2 0	in	0.10 ft		
Hose	Sanitary Tub Schedule: S	ing 2 TD	in	14.50 ft	3 x Elbow - L	ong radius, r/d 1.5 (90°)

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# Appendix G

Potable Water

# **1 DESCRIPTION**

This appendix documents the calculations used in designing the potable water system. These calculations were used to determine flow demand and pipe sizes for the potable water piping and to size the potable water pressure tank and pump.

# 2 PROCEDURE

Calculations are presented in the following sequence:

- Demand water supply calculation
- Potable water tank sizing calculation

System sizing is based on the guidance found in Appendix A of Reference [1].

# **3 GIVEN AND ASSUMED PARAMETERS**

- The system is to be pressurized by a single pump which will cycle on at 40psig and off at 60 psig.
- The heads will be Headhunter brand with less than 1 gpm per flush.
- The potable water consumers on the vessel: 2 heads, 2 lavatories, 1 sink in the food service area and 3 exterior hose bibs.

# 4 FORMULAS

The following formulas, taken from [2], are used to estimate the size of the potable water pressure tank:

Eq 1: Supplemental Drawdown (gal) = (Peak demand (gpm) – pump capacity(gpm)) × Peak Demand Time (min)

Eq 2: Total Pressure Tank Volume =  $\frac{Minimum Drawdown + Supplemental Drawdown}{Acceptance Factor}$ 

Eq 3: Acceptance Factor = 
$$1 - \frac{P1(tank \ precharge) + 14.7}{P2(cutout) + 14.7}$$

### **5** CALCULATIONS

#### 5.1 Demand Water Supply Calculations

			Water Supply Fixture	
Level	Item	Qty	Units, Table A-2	Item Totals
Main Deck	Food Service Sink	1	1.5	1.5
	Lavatory	2	1	2
	Hose Bib*	1	2.5	2.5
	Hose Bib	2	1	2
	Head	2	5	10
	Total, 03 Deck:			18
Total WSFU	for Vessel		18	
Supply dema	nd, from [1], Ch A-3, l	line 1	30	GPM
Excluding w	ater closets, from [1],	Ch A-3, Line 2	7	GPM
*First hose b	bib is 2.5 WSFU, addition	onal are 1.0		

Table 1: Water Supply

Demand flow from Chart A-3, Line 1 is 30 gpm, from [1]. This flow rate is for land side toilets that require 1.6 gpf. The toilets to be installed use less than 1 gpf. For a water system with 2 heads a 10 gpm at 50 psi would be sufficient, per [3].

#### 5.2 Pressure Tank Sizing Calculation

	Item	Qty		Note / Reference
(1)	Pump Capacity	10	gpm	
(2)	Minimum Drawdown	5	gallons	
(4)	Peak Demand Estimation	15	gpm	
(5)	Peak Demand Time	0.08	minutes	
(6)	P1 pressure tank precharge	40	psi	
(7)	P2 cutout pressure	60	psi	
(9)	Supplemental Drawdown	0.40	gallons	Eq. 1: [(4) - (1)] * (5)
(10)	Total Required Drawdown	5.40	gallons	Eq. 2: (2) + (9)
(11)	Acceptance Factor	0.27		Eq. 3: 1 - [[ (6) + 14.7 ]/[ (7) + 14.7 ]]
(12)	Total Calculated Tank Size	20	gallons	Eq. 4 (10)/(11)

Table 2: Pressure Tank Sizing

The toilet manufacture recommends a pressure tank with at least a 2 gallon draw down for a water system with 2 heads [3]. For approximately 5 gallon drawdown, a 20 gallon pressure tank is needed.

#### **6 REFERENCES**

- [1] IAPMO/ANSI UPC 1 2009: Uniform Plumbing Code, Ontario, CA: International Association of Plumbing and Mechanical Officials, 04/2009.
- [2] Water Systems Council, Wellcare Information For You About Sizing a Pressure Tank, Washington, DC.
- [3] Scott at Headhunter (2017, Jan. 13), *Headhunter Toilet Questions*, phone call, 01/13/17.